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(REV 11-98)

U.S. DEPARTMENT OF COMMERCE PATENT AND TRADEMARK OFFICE

ATTORNEY'S DOCKET NUMBER

TRANSMITTAL LETTER TO THE UNITED STATES

0264-0001

DESIGNATED/ELECTED OFFICE (DO/EO/US)

U.S. APPLICATION NO. (IF KNOWN, SEE 37 CFR

CONCERNING A FILING UNDER 35 U.S.C. 371

To Be Assigned 09/787668

INTERNATIONAL APPLICATION NO.

INTERNATIONAL FILING DATE

PRIORITY DATE CLAIMED

PCT/ZA99/00096

17-September-1999

05-October-1998 and 11-December-1998

TITLE OF INVENTION

Process for Producing Middle Distillates and Middle Distillates Produced By That Process

APPLICANT(S) FOR DO/EO/US

De Haan, et al.

Applicant herewith submits to the United States Designated/Elected Office (DO/EO/US) the following items and other information:

1. ☒ This is a **FIRST** submission of items concerning a filing under 35 U.S.C. 371.
2. ☐ This is a **SECOND** or **SUBSEQUENT** submission of items concerning a filing under 35 U.S.C. 371.
3. ☐ This is an express request to begin national examination procedures (35 U.S.C. 371(f)) at any time rather than delay examination until the expiration of the applicable time limit set in 35 U.S.C. 371(b) and PCT Articles 22 and 39(1).
4. ☒ A proper Demand for International Preliminary Examination was made by the 19th month from the earliest claimed priority date.
5. ☒ A copy of the International Application as filed (35 U.S.C. 371 (c) (2))
 - a. ☒ is transmitted herewith (required only if not transmitted by the International Bureau).
 - b. ☒ has been transmitted by the International Bureau.
 - c. ☐ is not required, as the application was filed in the United States Receiving Office (RO/US).
6. ☐ A translation of the International Application into English (35 U.S.C. 371(c)(2)).
7. ☒ A copy of the International Search Report (PCT/ISA/210).
8. ☐ Amendments to the claims of the International Application under PCT Article 19 (35 U.S.C. 371 (c)(3))
 - a. ☐ are transmitted herewith (required only if not transmitted by the International Bureau).
 - b. ☐ have been transmitted by the International Bureau.
 - c. ☐ have not been made; however, the time limit for making such amendments has NOT expired.
 - d. ☐ have not been made and will not be made.
9. ☐ A translation of the amendments to the claims under PCT Article 19 (35 U.S.C. 371(c)(3)).
10. ☐ An oath or declaration of the inventor(s) (35 U.S.C. 371 (c)(4)).
11. ☒ A copy of the International Preliminary Examination Report (PCT/IPEA/409).
12. ☐ A translation of the annexes to the International Preliminary Examination Report under PCT Article 36 (35 U.S.C. 371 (c)(5)).

Items 13 to 20 below concern document(s) or information included:

13. ☒ An Information Disclosure Statement under 37 CFR 1.97 and 1.98.
14. ☐ An assignment document for recording. A separate cover sheet in compliance with 37 CFR 3.28 and 3.31 is included.
15. ☒ A **FIRST** preliminary amendment.
16. ☐ A **SECOND** or **SUBSEQUENT** preliminary amendment.
17. ☐ A substitute specification.
18. ☐ A change of power of attorney and/or address letter.
19. ☐ Certificate of Mailing by Express Mail
20. ☒ Other items or information:

1. Copy of International Publication No. WO00/20535;
2. Copy of the PCT Request;
3. Notification Regarding the Confirmation of Precautionary Designations;
4. Notice of Confirmation of Precautionary Designations;
5. Form PCT/IB/301;
6. Form PCT/IB/304;
7. Form PCT/IB/308;
8. Form PCT/IB/332;
9. Copy of PCT Demand; and
10. Postcard.

U.S. APPLICATION NO. (IF KNOWN, SEE 37 CFR 1.53) 09/787668		INTERNATIONAL APPLICATION NO. PCT/ZA99/00096		ATTORNEY'S DOCKET NUMBER 0264-0001	
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21. The following fees are submitted:

BASIC NATIONAL FEE (37 CFR 1.492 (a) (1) - (5)) :				CALCULATIONS PTO USE ONLY	
<input type="checkbox"/>	Neither international preliminary examination fee (37 CFR 1.482) nor international search fee (37 CFR 1.445(a)(2)) paid to USPTO and International Search Report not prepared by the EPO or JPO	\$970.00			
<input checked="" type="checkbox"/>	International preliminary examination fee (37 CFR 1.482) not paid to USPTO but International Search Report prepared by the EPO or JPO	\$840.00			
<input type="checkbox"/>	International preliminary examination fee (37 CFR 1.482) not paid to USPTO but international search fee (37 CFR 1.445(a)(2)) paid to USPTO	\$690.00			
<input type="checkbox"/>	International preliminary examination fee paid to USPTO (37 CFR 1.482) but all claims did not satisfy provisions of PCT Article 33(1)-(4)	\$670.00			
<input type="checkbox"/>	International preliminary examination fee paid to USPTO (37 CFR 1.482) and all claims satisfied provisions of PCT Article 33(1)-(4)	\$96.00			
ENTER APPROPRIATE BASIC FEE AMOUNT =					
\$840.00					
Surcharge of \$130.00 for furnishing the oath or declaration later than <input type="checkbox"/> 20 <input type="checkbox"/> 30 months from the earliest claimed priority date (37 CFR 1.492 (e)).					
\$0.00					
CLAIMS	NUMBER FILED	NUMBER EXTRA	RATE		
Total claims	58 - 20 =	38	x \$18.00	\$684.00	
Independent claims	2 - 3 =	0	x \$78.00	\$0.00	
Multiple Dependent Claims (check if applicable).			<input checked="" type="checkbox"/>	\$260.00	
TOTAL OF ABOVE CALCULATIONS =				\$1,784.00	
Reduction of 1/2 for filing by small entity, if applicable. Verified Small Entity Statement must also be filed (Note 37 CFR 1.9, 1.27, 1.28) (check if applicable).			<input type="checkbox"/>	\$0.00	
SUBTOTAL =				\$1,784.00	
Processing fee of \$130.00 for furnishing the English translation later than <input type="checkbox"/> 20 <input type="checkbox"/> 30 months from the earliest claimed priority date (37 CFR 1.492 (f)).			+	\$0.00	
TOTAL NATIONAL FEE =				\$1,784.00	
Fee for recording the enclosed assignment (37 CFR 1.21(h)). The assignment must be accompanied by an appropriate cover sheet (37 CFR 3.28, 3.31) (check if applicable).			<input type="checkbox"/>	\$0.00	
TOTAL FEES ENCLOSED =				\$1,784.00	
				Amount to be: refunded	\$
				charged	\$

☒ A check in the amount of **\$1,784.00** to cover the above fees is enclosed.

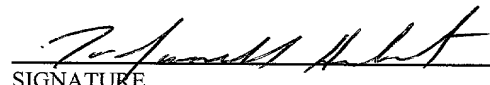
☐ Please charge my Deposit Account No. _____ in the amount of _____ to cover the above fees.
A duplicate copy of this sheet is enclosed.

☒ The Commissioner is hereby authorized to charge any fees which may be required, or credit any overpayment to Deposit Account No. **50-0622** A duplicate copy of this sheet is enclosed.

NOTE: Where an appropriate time limit under 37 CFR 1.494 or 1.495 has not been met, a petition to revive (37 CFR 1.137(a) or (b)) must be filed and granted to restore the application to pending status.

SEND ALL CORRESPONDENCE TO:

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 TransPotomac Plaza
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 SIGNATURE

Toni-Junell Herbert
 NAME

34,348
 REGISTRATION NUMBER

3/21/01
 DATE

IN THE UNITED STATES PATENT AND TRADEMARK OFFICE

In re Application of: De Haan, et al.

Art Unit: To Be Assigned

Serial No.: To Be Assigned

Examiner: To Be Assigned

Filed: Herewith

Atty. Docket: 0264-0001

For: Process for Producing Middle Distillates and
Middle Distillates Produced By That Process

PRELIMINARY AMENDMENT

Assistant Commissioner for Patents
Washington, D.C. 20231

Sir:

Prior to examination of the above-identified application, Applicants herewith respectfully requests the following amendments:

IN THE SPECIFICATION:

On page 2, line 1, of the international application, please insert the following paragraphs:

Further, WO 97/14769 discloses diesel fuels having excellent lubricity, oxidative stability and high cetane number produced from the non-shifting Fischer-Tropsch processes and having >95 wt% paraffins with an iso to normal ratio of from 0.3 to 3.0 . No mention is made regarding the effect of branching on the cold flow properties or the cetane number.

Still further, WO 98/34998 discloses a process for producing additive compositions, especially via a Fischer-Tropsch reaction, useful for improving the cetane number or lubricity of a middle distillate diesel fuel. The additive is prepared by fractionating the products of a Fischer-Tropsch reaction into a low boiling 371 degC

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fraction and a high boiling fraction, and hydroisomerising the high boiling fraction into a low boiling fraction and blending the low boiling fraction and the hydroisomerised high boiling fraction to produce the additive having >90 wt% C₁₆ to C₂₀ paraffins of which >50 wt% are isoparaffins. This disclosure does not disclose that a diesel fuel having good cold flow properties and high cetane number can be produced, only an additive, also the disclosure requires hydroisomerisation of a high boiling fraction which leads to a loss of material from the diesel boiling range into lighter material and to the formation of branched isomers, which leads to Cetane ratings less than the corresponding n-paraffins. The disclosure also does not address the issue of cold flow properties simultaneously with high a Cetane number.

Also on page 2 of the international application, please insert the following paragraph at line 16:

The synthetic middle distillate cut may include more than 50 mass% paraffins lighter than C₁₆.

On page 11 of the international application, please insert a line space between paragraphs 2 and 3 as indicated below:

The combination of highly linear paraffins derived from the <270°C fraction and mainly branched paraffins derived from the >270°C fraction results in a superb diesel.

Important parameters for a FT work-up process are maximization of product yield, product quality and cost. While the proposed process scheme is simple and therefore cost-effective, it produces High Performance Diesel, having a Cetane number >70, and naphtha in good yield. In fact, the process of this invention is able to produce a diesel of hitherto unmatched quality, which is characterized by a unique combination of both high Cetane number and excellent cold flow properties. This is believed to be related to a low degree of isomerisation in the 160-270°C fraction of the diesel and contrary to this, a high degree of isomerisation in the 270-370°C fraction of the diesel.

IN THE CLAIMS:

Please substitute the original claims 1-65 with the following claims as outlined:

1. A synthetic middle distillate cut comprising more than 50 mass% paraffins lighter than C₁₆ and in which more than 50 mass% of all paraffins of the middle distillate cut are isoparaffins, and wherein the isoparaffins are predominantly methyl and/or ethyl and/or propyl branched.
2. A synthetic middle distillate cut as claimed in claim 1, wherein the gradient of an isoparaffins to n-paraffins mass ratio profile of the synthetic middle distillate cut increases from about 1:1 for C₈ to 8.54:1 for C₁₅ and decrease again to about 3:1 for C₁₈.
3. A synthetic middle distillate cut as claimed in claim 1, wherein a fraction of the synthetic middle distillate cut in the C₁₀ to C₁₈ carbon number range has a higher ratio of isoparaffins to n-paraffins than a C₈ to C₉ fraction of the synthetic middle distillate cut.
4. A synthetic middle distillate cut as claimed in claim 3, wherein the isoparaffins to n-paraffins mass ratio of the C₁₀ to C₁₈ fraction is between 1:1 and 9:1.
5. A synthetic middle distillate cut as claimed in claim 3, wherein a C₁₉ to C₂₄ fraction of the middle distillate cut has a mass ratio range of isoparaffins to n-paraffins of from 3.3:1 to 5:1.
6. A synthetic middle distillate cut as claimed in claim 5, wherein the C₁₉ to C₂₄ fraction of the middle distillate cut has a mass ratio range of isoparaffins to n-paraffins of between 4:1 and 4.9:1.
7. A synthetic middle distillate cut as claimed in claim 3, which comprises 30 mass% of a straight run component thereby selecting the isoparaffins to n-paraffins mass ratio of the C₁₀ to C₁₈ fraction to between 1:1 and 2:5:1.
8. A synthetic middle distillate cut as claimed in claim 3, which comprises 20 mass% of a straight run component thereby selecting the isoparaffins to n-paraffins mass ratio of the C₁₀ to C₁₈ fraction to between 1.5:1 and 3:5:1.

9. A synthetic middle distillate cut as claimed in claim 3, which comprises 10 mass% of a straight run component thereby selecting the isoparaffins to n-paraffins mass ratio of the C₁₀ to C₁₈ fraction to between 2.3:1 and 4.3:1.
10. A synthetic middle distillate cut as claimed in claim 3, wherein the isoparaffins to n-paraffins mass ratio of the C₁₀ to C₁₈ fraction having substantially only a hydrocracked component is between 4:1 and 9:1.
11. A middle distillate cut as claimed in claim 1, wherein at least some of the isoparaffins are di-methyl branched.
12. A middle distillate cut as claimed in claim 1, wherein at least 30 mass% of the isoparaffins are mono-methyl branched.
13. A middle distillate cut as claimed in claim 1, wherein at least some of the isoparaffins are ethyl branched.
14. A middle distillate cut as claimed in claim 1, wherein the ratio of isoparaffins to n-paraffins of the middle distillate cut is from about 1:1 to about 12:1.
15. A synthetic middle distillate cut as claimed in claim 14, wherein the isoparaffins to n-paraffins mass ratio is between about 2:1 to about 6:1.
16. A synthetic middle distillate cut as claimed in claim 15, wherein the isoparaffins to n-paraffins mass ratio is 4:1.
17. A synthetic middle distillate cut as claimed in claim 3, having a light fraction in the boiling range 160°C to 270°C wherein the isoparaffins to n-paraffins mass ratio of the light fraction is from 1:2 to 4:1.
18. A synthetic middle distillate cut as claimed in claim 17, having the light fraction in the boiling range 160°C to 270°C wherein the isoparaffins to n-paraffins mass ratio of the light fraction is 2.2:1.
19. A synthetic middle distillate cut as claimed in claim 3, having a heavy fraction in the boiling range 270°C to 370°C wherein the isoparaffins to n-paraffins mass ratio of the heavy fraction is from 4:1 to 14:1.
20. A synthetic middle distillate cut as claimed in claim 19, having the heavy fraction in the boiling range 270°C to 370°C wherein the isoparaffins to n-paraffins mass ratio of the heavy fraction is 21:2.

21. A synthetic middle distillate cut as claimed in claim 1 , wherein the synthetic distillate is derived from one or more FT primary product.
22. A synthetic middle distillate cut as claimed in claim 3, wherein the synthetic distillate is derived from one or more FT primary product.
23. A synthetic middle distillate cut as claimed in claim 5, wherein the synthetic distillate is derived from one or more FT primary product.
24. A diesel fuel composition including from 10% to 100% of a middle distillate cut as claimed in claim 1.
25. A diesel fuel composition including from 10% to 100% of a middle distillate cut as claimed in claim 3.
26. A diesel fuel composition including from 10% to 100% of a middle distillate cut as claimed in claim 5.
27. A diesel fuel composition as claimed in claim 26, including from 0 to 90% of one or more other diesel fuel.
28. A diesel fuel composition as claimed in claim 26, including from 20 to 80% of one or more other diesel fuel.
29. A diesel fuel composition as claimed in claim 28, including at least 20% of the middle distillate cut, the composition having a Cetane number greater than 47 and a CFPP, in accordance with IP 309, below -22°C .
30. A diesel fuel composition as claimed in claim 28, including at least 30% of the middle distillate cut, the composition having a Cetane number greater than 50 and a CFPP, in accordance with IP 309, below -22°C .
31. A diesel fuel composition as claimed in claim 28, including at least 50% of the middle distillate cut, the composition having a Cetane number greater than 52 and a CFPP, in accordance with IP 309, below -25°C .
32. A diesel fuel composition as claimed in claim 28, including at least 70% of the middle distillate cut, the composition having a Cetane number greater than 60 and a CFPP, in accordance with IP 309, below -30°C .
33. A diesel fuel composition as claimed in claim 26, including from 0 to 10% additives.

34. A diesel fuel composition as claimed in claim 33, wherein the additives include a lubricity improver.
35. A diesel fuel composition as claimed in claim 27, wherein one of the other diesel fuels is US 2-D grade diesel fuel.
36. A diesel fuel composition as claimed in claim 27, wherein one of the other diesel fuels is CARB grade diesel fuel.
37. A process for producing a synthetic middle distillate having a Cetane number higher than 70, the process including:
 - (a) separating the products obtained from synthesis gas via a FT synthesis reaction into one or more heavier fraction and one or more lighter fraction;
 - (b) catalytically processing the heavier fraction under conditions which yield mainly middle distillates;
 - (c) separating the middle distillate product of step (b) from a light product fraction and a heavier product fraction which are also produced in step (b); and
 - (d) blending the middle distillate fraction obtained in step (c) with at least a portion of the one or more lighter fraction of step (a), or products thereof.
38. A process for producing a synthetic middle distillate as claimed in claim 37, wherein the catalytic processing of step (b) is a hydroprocessing step.
39. A process for producing a synthetic middle distillate as claimed in claim 38, wherein the catalytic processing of step (b) is a hydrocracking step.
40. A process for producing a synthetic middle distillate as claimed in claim 37, including one or more additional step of fractionating at least some of the one or more lighter fraction of step (a), or products thereof, prior to step (d).
41. A process for producing a synthetic middle distillate as claimed in claim 37, including the additional step of hydrotreating at least some of the one or more light fraction of step (a), or products thereof, prior to step (d).
42. A process for producing a synthetic middle distillate as claimed in claim 39, including the additional step of hydrotreating at least some of the one or more light fraction of step (a), or products thereof, prior to step (d).

43. A process for producing a synthetic middle distillate as claimed in claim 37, wherein the one or more heavier fraction of step (a) boils above about 270°C.
44. A process for producing a synthetic middle distillate as claimed in claim 39, wherein the one or more heavier fraction of step (a) boils above about 270°C.
45. A process for producing a synthetic middle distillate as claimed in 43, wherein the one or more heavier fraction of step (b) has a isoparaffins to n-paraffins mass ratio of between 4:1 and 14:1.
46. A process for producing a synthetic middle distillate as claimed in 44, wherein the one or more heavier fraction of step (b) has a isoparaffins to n-paraffins mass ratio of 21:2.
47. A process for producing a synthetic middle distillate as claimed in claim 37, wherein the one or more heavier fraction of step (a) boils above about 300°C.
48. A process for producing a synthetic middle distillate as claimed in claim 37, wherein the one or more lighter fraction boils in the range C₅ to the boiling point of the heavier fraction.
49. A process for producing a synthetic middle distillate as claimed in claim 48, wherein the one or more lighter fraction boils in the range 160°C to 270°C.
50. A process for producing a synthetic middle distillate as claimed in claim 48, wherein the one or more lighter fraction has an isoparaffins to n-paraffins mass ratio of between 1:2 and 4:1.
51. A process for producing a synthetic middle distillate as claimed in claim 50, wherein the one or more lighter fraction has an isoparaffins to n-paraffins mass ratio of 2.2:1.
52. A process for producing a synthetic middle distillate as claimed in claim 37, wherein the product of step (d) boils in the range 100°C to 400°C.
53. A process for producing a synthetic middle distillate as claimed in claim 37, wherein the product of step (d) boils in the range 160°C to 370°C.
54. A process for producing a synthetic middle distillate as claimed in claim 37, wherein the product of step (d) is a diesel fuel which has a CFPP below -20°C.

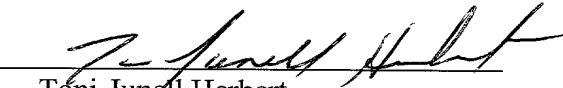
55. A process for producing a synthetic middle distillate as claimed in claim 54, wherein the product of step (d) is obtained by mixing the middle distillate fraction obtained in step (c) with at least a portion of the one or more lighter fraction of step (a), or products thereof, in a volume ratio selected to provide a diesel fuel having a required specification.
56. A process for producing a synthetic middle distillate as claimed in claim 55, wherein the product of step (d) is obtained by mixing the middle distillate fraction obtained in step (c) with at least a portion of the one or more lighter fraction of step (a), or products thereof, in a volume ratio of between 1:1 and 9:1.
57. A process for producing a synthetic middle distillate as claimed in claim 56, wherein the product of step (d) is obtained by mixing the middle distillate fraction obtained in step (c) with at least a portion of the one or more lighter fraction of step (a), or products thereof, in a volume ratio of between 2:1 and 6:1.
58. A process for producing a synthetic middle distillate as claimed in claim 55 to 60, wherein the product of step (d) is obtained by mixing the middle distillate fraction obtained in step (c) with at least a portion of the one or more lighter fraction of step (a), or products thereof, in a volume ratio of 84:16.

REMARKS

A marked-up version of the amendments is enclosed for your reference. It is respectfully requested that the Examiner enter these amendments prior to examining the application on its merits.

Respectfully submitted,

SHANKS & HERBERT

By: 
Toni-June Herbert
Reg. No. 34,348

Date: 3/21/01

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**PROCESS FOR PRODUCING MIDDLE DISTILLATES AND MIDDLE DISTILLATES
PRODUCED BY THAT PROCESS**

Field of the Invention

This invention relates to middle distillates having good cold flow properties, such as the Cold Filter Plugging Point (CFPP) measured in accordance with the IP method 309, and a high Cetane number, as well as to a process for production of such distillates. More particularly, this invention relates to middle distillates produced from a mainly paraffinic synthetic crude which is produced by the reaction of CO and H₂, typically by the Fischer-Tropsch (FT) process.

Background to the invention

Waxy products of a FT hydrocarbon synthesis process, particularly the products of a cobalt and/or iron based catalytic process, contain a high proportion of normal paraffins. Primary FT products provide notoriously poor cold flow properties, making such products difficult to use where cold flow properties are vital, e.g. diesel fuels, lube oil bases and jet fuel. It is known in the art that cold flow properties of a middle distillate, such as jet fuel, can be improved by increasing the branching of the paraffins of distillates within the proper boiling range, as well as by hydrocracking and hydroisomerising heavier components. Hydrocracking, however, produces smaller amounts of gases and light products, which reduce the yield of valuable distillates. There remains an incentive for a process to maximize middle distillates obtained from FT waxes having good cold flow properties and a high Cetane number.

The middle distillate fuel described in this invention is produced from a highly paraffinic synthetic crude (syncrude) obtained from synthesis gas (syngas) through a reaction like the FT reaction. The FT primary products cover a broad range of hydrocarbons from methane to species with molecular masses above 1400; including mainly paraffinic hydrocarbons and much smaller quantities of other species such as olefins, and oxygenates.

The prior art teaches in US 5,378,348 that by hydrotreating and isomerizing the products from a Fisher-Tropsch reactor one can obtain a jet fuel with freezing point of -34°C or lower due to the iso-paraffinic nature of this fuel. This increased product branching relative to the waxy paraffin feed corresponds with a Cetane rating (combustion) value less than that for normal (linear) paraffins, depicting that an increase in branching reduces the Cetane value of paraffinic hydrocarbon fuels.

Surprisingly, it has now been found by the applicant, that a hydroprocessed middle distillate, such as diesel, may be produced having a high Cetane number as well as good cold flow properties. The middle distillates of the present invention could be used on their own or in blends to improve the quality of other diesel fuels not meeting the current and/or proposed, more stringent fuel quality specifications.

Summary of the invention

Thus, according to a first aspect of the invention, there is provided a process for the production of a middle distillate or distillate blend, such as diesel, having a high Cetane number as well as good cold flow properties.

The synthetic middle distillate cut may comprise more than 50% isoparaffins, wherein the isoparaffins are predominantly methyl and/or ethyl and/or propyl branched.

The gradient of an isoparaffins to n-paraffins mass ratio profile of the synthetic middle distillate cut may increase from about 1:1 for C₈ to 8.54:1 for C₁₅ and decrease again to about 3:1 for C₁₈.

Typically, a fraction of the synthetic middle distillate cut in the C₁₀ to C₁₈ carbon number range has a higher ratio of isoparaffins to n-paraffins than a C₈ to C₉ fraction of the synthetic middle distillate cut.

The isoparaffins to n-paraffins mass ratio of the C₁₀ to C₁₈ fraction may be between 1:1 and 9:1.

The isoparaffins to n-paraffins mass ratio may be 8.54:1 for a C₁₅ fraction of the synthetic middle distillate cut.

A C₁₉ to C₂₄ fraction of the middle distillate cut may have a narrow mass ratio range of isoparaffins to n-paraffins of between 3.3:1 and 5:1, generally between 4:1 and 4.9:1.

The mass ratio of isoparaffins to n-paraffins may be adjusted by controlling the blend ratio of hydrocracked to straight run components of the synthetic middle distillate cut. Thus, the isoparaffins to n-paraffins mass ratio of the C₁₀ to C₁₈ fraction having 30% straight run component may be between 1:1 and 2.5:1.

The isoparaffins to n-paraffins mass ratio of the C₁₀ to C₁₈ fraction having 20% straight run component may be between 1.5:1 and 3:5:1.

The isoparaffins to n-paraffins mass ratio of the C₁₀ to C₁₈ fraction having 10% straight run component may be between 2.3:1 and 4.3:1.

The isoparaffins to n-paraffins mass ratio of the C₁₀ to C₁₈ fraction having substantially only a hydrocracked component may be between 4:1 and 9:1.

At least some of the isoparaffins may be methyl branched. At least some of the isoparaffins may be dimethyl branched. At least 30% (mass) of the isoparaffins are typically mono-methyl branched.

Some of the isoparaffins may however be ethyl branched.

Table A: Comparison of the Branching Characteristics of Blends of SR, HX and SPD Diesels

	SR Diesel			HX Diesel			SPD-Diesel		
	n-Paraff	I-Paraff	Total	n-Paraff	I-Paraff	Total	n-Paraff	I-Paraff	Total
C8	1.07		1.07	0.38		0.38	0.58		0.58
C9	22.64	1.57	24.21	1.86	5.37	7.23	6.01	3.60	9.61
C10	14.73	1.74	16.47	1.90	8.43	10.33	6.48	6.12	12.60
C11	5.43	0.32	5.75	1.60	8.75	10.35	6.13	6.31	12.44
C12	11.79	0.67	12.46	1.41	8.88	10.29	6.57	5.94	12.51
C13	11.16	0.65	11.81	1.32	8.46	9.78	6.31	6.03	12.34
C14	11.66	0.70	12.36	1.27	8.95	10.22	6.41	5.82	12.23
C15	9.19	0.46	9.65	1.03	8.80	9.83	4.98	4.97	9.95
C16	4.94	0.31	5.25	0.96	6.38	7.34	2.58	3.53	6.11
C17	0.88		0.88	0.88	3.92	4.80	0.76	2.33	3.09
C18	0.08		0.08	0.90	2.73	3.63	0.66	1.93	2.59
C19				0.60	2.69	3.29	0.38	1.47	1.85
C20				0.54	2.38	2.92	0.32	0.78	1.10
C21				0.56	2.73	3.29	0.29	0.72	1.01
C22				0.60	2.12	2.72	0.29	0.53	0.82
C23				0.41	1.93	2.34	0.25	0.40	0.65
C24				0.23	0.92	1.15	0.16	0.38	0.54
C25					0.14	0.14			
Total	93.57	6.42	99.99	16.45	83.58	100.03	49.16	50.86	100.02

In the table: SPD – Sasol Slurry Phase Distillate

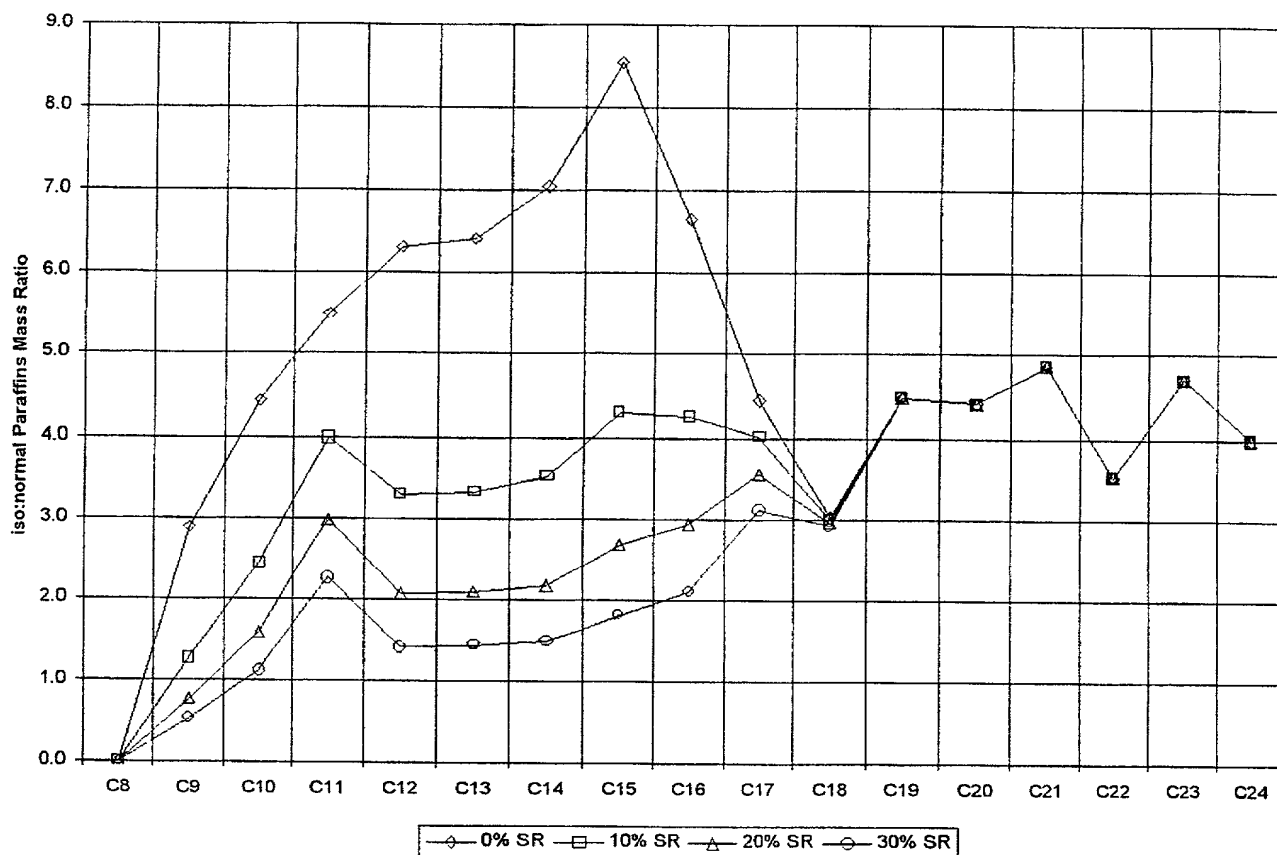
SR – Straight Run

HX – Hydrocracked

Table B: Branching Characteristics of Blends of SR & HX Diesels

SR Diesel (mass)	iso:normal Paraffins Ratio (mass)			
	0%	10%	20%	30%
C8	0.0	0.0	0.0	0.0
C9	2.9	1.3	0.8	0.5
C10	4.4	2.4	1.6	1.1
C11	5.5	4.0	3.0	2.3
C12	6.3	3.3	2.1	1.4
C13	6.4	3.3	2.1	1.4
C14	7.0	3.5	2.2	1.5
C15	8.5	4.3	2.7	1.8
C16	6.6	4.3	2.9	2.1
C17	4.5	4.0	3.6	3.1
C18	3.0	3.0	3.0	2.9
C19	4.5	4.5	4.5	4.5
C20	4.4	4.4	4.4	4.4
C21	4.9	4.9	4.9	4.9
C22	3.5	3.5	3.5	3.5
C23	4.7	4.7	4.7	4.7
C24	4.0	4.0	4.0	4.0
C25				

Branching Characteristics of FT Diesel



According to a further aspect of the invention, there is provided a synthetic middle distillate cut having a Cetane number above 70 and a CFPP, in accordance with IP 309, of below -20°C , said distillate having an isoparaffinic content substantially as described above.

5

In one embodiment, the synthetic middle distillate cut is a FT product.

The invention extends to a diesel fuel composition including from 10% to 100% of a middle distillate cut as described above.

10

Typically, the diesel fuel composition may include from 0 to 90% of one or more other diesel fuel.

The diesel fuel composition may include at least 20% of the middle distillate cut, the composition having a Cetane number greater than 47 and a CFPP, in accordance with IP 309, below -22°C .

15 The diesel fuel composition may include at least 30% of the middle distillate cut, the composition having a Cetane number greater than 50 and a CFPP, in accordance with IP 309, below -22°C .

The diesel fuel composition may include at least 50% of the middle distillate cut, the composition having a Cetane number greater than 52 and a CFPP, in accordance with IP 309, below -25°C .

- 5 The diesel fuel composition may include at least 70% of the middle distillate cut, the composition having a Cetane number greater than 60 and a cold flow plug point, in accordance with IP 309, below -30°C .

The diesel fuel composition may further include from 0 to 10% additives.

10

The additives may include a lubricity improver.

The lubricity improver may comprise from 0 to 0.5% of the composition, typically from 0.00001% to 0.05% of the composition. In some embodiments, the lubricity improver comprises from 0.008% to 0.02% of the composition.

15

The diesel fuel composition may include, as the other diesel, a crude oil derived diesel, such as US 2-D grade (low sulphur No. 2-D grade for diesel fuel oil as specified in ASTM D 975-94) and/or CARB (California Air Resources Board 1993 specification) diesel fuel.

20

According to yet another aspect of the invention, there is provided a process for producing a synthetic middle distillate having a Cetane number higher than 70, the process including:

- (a) separating the products obtained from synthesis gas via the FT synthesis reaction into one or more heavier fraction and one or more lighter fraction;
- 25 (b) catalytically processing the heavier fraction under conditions which yield mainly middle distillates;
- (c) separating the middle distillate product of step (b) from a light product fraction and a heavier product fraction which are also produced in step (b); and
- (d) blending the middle distillate fraction obtained in step (c) with at least a portion of the one or
- 30 more lighter fraction of step (a), or products thereof.

The catalytic processing of step (b) may be a hydroprocessing step, for example, hydrocracking.

The process for producing a synthetic middle distillate may include one or more additional step of

35 fractionating at least some of the one or more lighter fraction of step (a), or products thereof, prior to step (d).

The process for producing a synthetic middle distillate may include the additional step of hydrotreating at least some of the one or more light fraction of step (a), or products thereof, prior to step (d).

5 The one or more heavier fraction of step (a) may have a boiling point above about 270°C, however, it may be above 300°C.

The one or more lighter fraction may have a boiling point in the range C₅ to the boiling point of the heavier fraction, typically in the range 160°C to 270°C.

10 The product of step (d) may boil in the range 100°C to 400°C. The product of step (d) may boil in the range 160°C to 370°C.

The product of step (d) may be a diesel fuel.

15 The product of step (d) may have a CFPP below -20°C, typically below -30°C, and even below -35°C.

20 The product of step (d) may be obtained by mixing the middle distillate fraction obtained in step (c) with at least a portion of the one or more lighter fraction of step (a), or products thereof, in a volume ratio of between 1:1 and 9:1, typically 2:1 and 6:1, and in one embodiment, in a volume ratio of 84:16.

25 The invention extends further to a process for the production of middle distillate fuels from FT primary products, comprising predominantly long chain linear paraffins.

30 In this process, the waxy product from the FT process is separated into at least two fractions, a heavier and at least one lighter fraction. The lighter fraction may be subjected to mild catalytic hydrogenation to remove hetero-atomic compounds such as oxygen and to saturate olefins, thereby producing material useful as naphtha, solvents, diesel and/or blending components therefor. The heavier fraction may be catalytically hydroprocessed without prior hydrotreating to produce products with good cold flow characteristics. This hydroprocessed heavier fraction could be blended with all or part of the hydrogenated and/or unhydrogenated light fraction to obtain, after fractionation, naphtha and a diesel fuel characterised by a high Cetane number.

The catalysts suitable for the hydroprocessing steps are commercially available and can be selected towards an improved quality of the desired final product.

Detailed Description

5

This invention describes the conversion of primary FT products into naphtha and middle distillates, for example, diesel having a high Cetane number in excess of 70, while also having good cold flow properties, as described above.

10

The FT process is used industrially to convert synthesis gas, derived from coal, natural gas, biomass or heavy oil streams, into hydrocarbons ranging from methane to species with molecular masses above 1400.

15

While the main products are linear paraffinic materials, other species such as branched paraffins, olefins and oxygenated components form part of the product slate. The exact product slate depends on reactor configuration, operating conditions and the catalyst that is employed, as is evident from e.g. Catal.Rev.-Sci. Eng., 23(1&2), 265-278 (1981).

20

Preferred reactors for the production of heavier hydrocarbons are slurry bed or tubular fixed bed reactors, while operating conditions are preferably in the range of 160°C – 280°C, in some cases 210-260°C, and 18 – 50 Bar, in some cases 20-30 bar.

25

Preferred active metals in the catalyst comprise iron, ruthenium or cobalt. While each catalyst will give its own unique product slate, in all cases the product slate contains some waxy, highly paraffinic material which needs to be further upgraded into usable products. The FT products can be converted into a range of final products, such as middle distillates, gasoline, solvents, lube oil bases, etc. Such conversion, which usually consists of a range of processes such as hydrocracking, hydrotreatment and distillation, can be termed a FT work-up process.

30

The FT work-up process of this invention uses a feed stream consisting of C₅ and higher hydrocarbons derived from a FT process. This feed is separated into at least two individual fractions, a heavier and at least one lighter fraction. The cut point between the two fractions is preferably less than 300°C and typically around 270°C.

35

The table below gives a typical composition of the two fractions, with a ±10% accuracy:

Table 1: Typical Fischer-Tropsch product after separation into two fractions (vol% distilled)

	Condensate (< 270°C fraction)	Wax (> 270°C fraction)
C ₅ -160°C	45	
160-270°C	51	3
270-370°C	4	35
370-500°C		42
> 500°C		20

The >270°C fraction, also referred to as wax, contains a considerable amount of hydrocarbon material, which boils higher than the normal diesel range. If we consider a typical diesel boiling range of 160-370°C, it means that all material heavier than 370°C needs to be converted into lighter materials by means of a catalytic process often referred to as hydroprocessing, for example, hydrocracking.

Catalysts for this step are of the bifunctional type; i.e. they contain sites active for cracking and for hydrogenation. Catalytic metals active for hydrogenation include group VIII noble metals, such as platinum or palladium, or a sulphided Group VIII base metals, e.g. nickel, cobalt, which may or may not include a sulphided Group VI metal, e.g. molybdenum. The support for the metals can be any refractory oxide, such as silica, alumina, titania, zirconia, vanadia and other Group III, IV, VA and VI oxides, alone or in combination with other refractory oxides. Alternatively, the support can partly or totally consist of zeolite. However, for this invention the preferred support is amorphous silica-alumina.

Process conditions for hydrocracking can be varied over a wide range and are usually laboriously chosen after extensive experimentation to optimize the yield of middle distillates. In this regard, it is important to note that, as in many chemical reactions, there is a trade-off between conversion and selectivity. A very high conversion will result in a high yield of gases and low yield of distillate fuels. It is therefore important to painstakingly tune the process conditions in order to limit the conversion of >370°C hydrocarbons. Table 2 gives a list of the preferred conditions.

Table 2: Process conditions for hydrocracking

CONDITION	BROAD RANGE	PREFERRED RANGE
Temperature, °C	150-450	340-400
Pressure, barg	10-200	30-80
Hydrogen Flow Rate, m ³ _n /m ³ feed	100-2000	800-1600
Conversion of >370°C material, mass %	30-80	50-70

Nevertheless, it is possible to convert all the >370°C material in the feedstock by recycling the part that is not converted during the hydrocracking process.

As is evident from table 1, most of the fraction boiling below 270°C is already in the typical boiling range for diesel, i.e. 160-370°C. This fraction may or may not be subjected to hydrotreating. By hydrotreating, hetero-atoms are removed and unsaturated compounds are hydrogenated. Hydrotreating is a well-known industrial process, catalyzed by any catalyst having a hydrogenation function, e.g. Group VIII noble metal or sulphided base metal or Group VI metals, or combinations thereof. Preferred supports are alumina and silica.

Table 3 gives typical operating conditions for the hydrotreating process.

Table 3: Operating conditions for the hydrotreating process.

CONDITION	BROAD RANGE	PREFERRED RANGE
Temperature, °C	150-450	200-400
Pressure, bar(g)	10-200	30-80
Hydrogen Flow Rate, m ³ _n /m ³ feed	100-2000	400-1600

While the hydrotreated fraction may be fractionated into paraffinic materials useful as solvents, the applicant has now surprisingly found that the hydrotreated fraction may be directly blended with the

products obtained from hydrocracking the wax. Although it is possible to hydroisomerise the material contained in the condensate stream, the applicant has found that this leads to a small, but significant loss of material in the diesel boiling range to lighter material. Furthermore, isomerisation leads to the formation of branched isomers, which leads to Cetane ratings less than that of the corresponding normal paraffins.

The combination of highly linear paraffins derived from the <270°C fraction and mainly branched paraffins derived from the >270°C fraction results in a superb diesel.

Important parameters for a FT work-up process are maximization of product yield, product quality and cost. While the proposed process scheme is simple and therefore cost-effective, it produces High Performance Diesel, having a Cetane number >70, and naphtha in good yield. In fact, the process of this invention is able to produce a diesel of hitherto unmatched quality, which is characterized by a unique combination of both high Cetane number and excellent cold flow properties. This is believed to be related to a low degree of isomerisation in the 160-270°C fraction of the diesel and contrary to this, a high degree of isomerisation in the 270-370°C fraction of the diesel.

The total amount of isomers in the light boiling range of the diesel (160-270°C fraction) and the heavier range of the diesel (270°C-370°C) are shown in the following table 4.

Table 4: Isoparaffins: n-Paraffins of Middle Distillate Fractions

Boiling Range	Corresponding Carbon Range	Average Iso:Normal Paraffins Ratio	
		Range	Typical value
160-270°C	C ₁₀ -C ₁₇	0.5 - 4.0	2.2
270-370°C	C ₁₇ -C ₂₃	4.0 - 14.0	10.5

The relatively high percentage of normal paraffins in the light boiling range contributes to the high Cetane number of the diesel fuel, without affecting the cold flow properties. On the other hand, in the heavier range of the diesel, branching is of utmost importance because the linear hydrocarbons in this range provide very poor cold flow properties and in some cases, may even crystallize. Therefore, the amount of iso-paraffins in this range is maximised during hydroprocessing under the process conditions described herein.

It is this unique composition of the synthetic fuel, which is directly caused by the way in which the FT work-up process of this invention is operated, that leads to the unique characteristics of said fuel.

The applicant has also found, that from the perspective of fuel quality, it is not necessary to hydrotreat the <270°C fraction, adding said fraction directly to the products from hydrocracking the wax. While

this results in the inclusion of oxygenates and unsaturates in the final diesel. fuel specifications usually allow for this. Circumventing the need for hydrotreatment of the condensate results in considerable savings of capital and operating costs.

- 5 The described FT work-up process of Figure 1 may be combined in a number of configurations. The applicant considers these an exercise in what is known in the art as Process Synthesis Optimisation.

However, the specific process conditions for the Work-up of FT primary products , the possible process configurations of which are outlined in Table 5, were obtained after extensive and laborious
10 experimentation and design.

Table 5 - Possible Fischer-Tropsch Product Work-up Process Configurations

Process Step		Process Configuration					
		A	B	C	D	E	F
2	Light FT Product Fractionator			X			X
3	Light FT Product Hydrotreater	X	X			X	X
4	Hydrotreater Products Fractionator		X			X	X
5	Waxy FT Product Hydrocracker	X	X	X	X	X	X
6	Hydrocracked Products Fractionator	X	X	X	X	X	X

15 Numbers reference numerals of Figure 1

FT Fischer-Tropsch

The basic process is outlined in the attached Figure 1. The synthesis gas (syngas), a mixture of Hydrogen and Carbon monoxide, enters the FT reactor 1 where the synthesis gas is converted to
20 hydrocarbons by the FT reaction.

A lighter FT fraction is recovered in line 7, and may or may not pass through fractionator 2 and hydrotreater 3. The product 9 from the hydrotreater may be separated in fractionator 4 or, alternatively, mixed with hydrocracker products 16 sent to a common fractionator 6.

25 A waxy FT fraction is recovered in line 13 and sent to hydrocracker 5. If fractionation 2 is considered the bottoms cut 12 are be sent to hydrocracker 5. The products 16, on their own or mixed with the lighter fraction 9a, are separated in fractionator 6.

Depending on the process scheme, a light product fraction, naphtha 19, is obtained from fractionator 6 or by blending equivalent fractions 10 and 17. This is a C₅-160°C fraction useful as naphtha.

A somewhat heavier cut, synthetic diesel 20, is obtainable in a similar way from fractionator 6 or by blending equivalent fractions 11 and 18. This cut is recovered as a 160-370°C fraction useful as diesel.

The heavy unconverted material 21 from fractionator 6 is recycled to extinction to hydrocracker 5. Alternatively, the residue may be used for production of synthetic lube oil bases. A small amount of C₁-C₄ gases are also separated in fractionator 6.

The following examples will serve to illustrate further this invention.

Examples

EXAMPLE 1

A commercially available hydrocracking catalyst was used for hydrocracking of a non-hydrotreated FT hydrocarbon fraction with an initial boiling point of about 280°C. The active metals on the catalyst comprised cobalt and molybdenum, while the support was amorphous silica-alumina. Operating conditions were temperatures between 375 and 385°C, pressure of 70 bar and hydrogen flow rate of 1500 m³_n/m³ feed. The experiment was carried out in a pilot plant reactor. The conversion of >370°C material to lighter material ranged between 65 and 80%. Diesel component A is obtained after fractionation of the reactor products. The properties of this diesel component are given in table 1.

EXAMPLE 2

A non-hydrotreated FT hydrocarbon fraction with a final boiling point of ca 285°C and alcohol content of ca. 4.3 mass%, expressed as n-hexanol, was rigorously hydrotreated using a commercially available catalyst. The active metals on the catalyst comprised molybdenum and cobalt, while the support was alumina. The process conditions were temperatures around 250°C, pressure of 68 bar and hydrogen flow rate of 1070 m³_n/m³ feed. The test was carried in a commercial scale fixed bed reactor. Diesel components B and C were obtained after fractionation of respectively the reactor feed and reactor product. The properties of these diesel components are given in table 6.

Table 6: Diesel Blending Components

	<i>Component A</i>	<i>Component B</i>	<i>Component C</i>
ASTM D86 distillation			
IBP, °C	185	161	186
10%, °C	211	188	198
50%, °C	269	224	223
90%, °C	338	263	259
FBP, °C	361	285	279
Density, kg/dm ³ @20°C	0.7766	0.7641	0.7515
Viscosity, cSt @ 40°C	2.66	1.81	1.54
Flash Point, °C	76	61	72
Cold Filter Plugging Point, °C	-32	-18	-17
Cetane Number	69	71	>74

EXAMPLE 3

The diesel fraction obtained from hydrocracking a heavy FT material (component A) was blended with a hydrogenated lighter FT material (component B) in a volume ratio of 84:16. The properties of the final blend, called Blend I, are given in table 7.

Those skilled in the art will realize that Blend I may be used on its own, but also as a blending feedstock. The combination of a high Cetane numbers, above 70, and excellent cold flow properties, with CFPP substantially better than -20°C, make Blend I an ideal blending feedstock to upgrade crude oil derived diesels.

EXAMPLE 4

The diesel fraction obtained from hydrocracking a heavy FT material (component A) was directly blended with a lighter non-hydrogenated FT material (component C) in a volume ratio of 84:16. The properties of the final blend, called Blend II, are given in table 7.

Similar to example 3, Blend II may be used on its own, but also as a blending feedstock. In addition to a high Cetane numbers, above 70, and excellent cold flow properties, with CFPP substantially better than -20°C . Blend II contains alcohols and smaller quantities of other oxygenates, the level of which depend on the blending ratio used to prepare the blend.

Table 7: Diesel Blends

	<i>Blend I</i>	<i>Blend II</i>
ASTM D86 distillation		
IBP, $^{\circ}\text{C}$	189	185
10%, $^{\circ}\text{C}$	209	208
50%, $^{\circ}\text{C}$	256	257
90%, $^{\circ}\text{C}$	331	332
FBP, $^{\circ}\text{C}$	356	358
Density, kg/dm^3 @ 15°C	0.7769	0.7779
Viscosity, cSt @ 40°C	2.43	2.42
Flash Point, $^{\circ}\text{C}$	73	67
Cold Filter Plugging Point, $^{\circ}\text{C}$	-37	-34
Cetane Number	>73.7	73.3

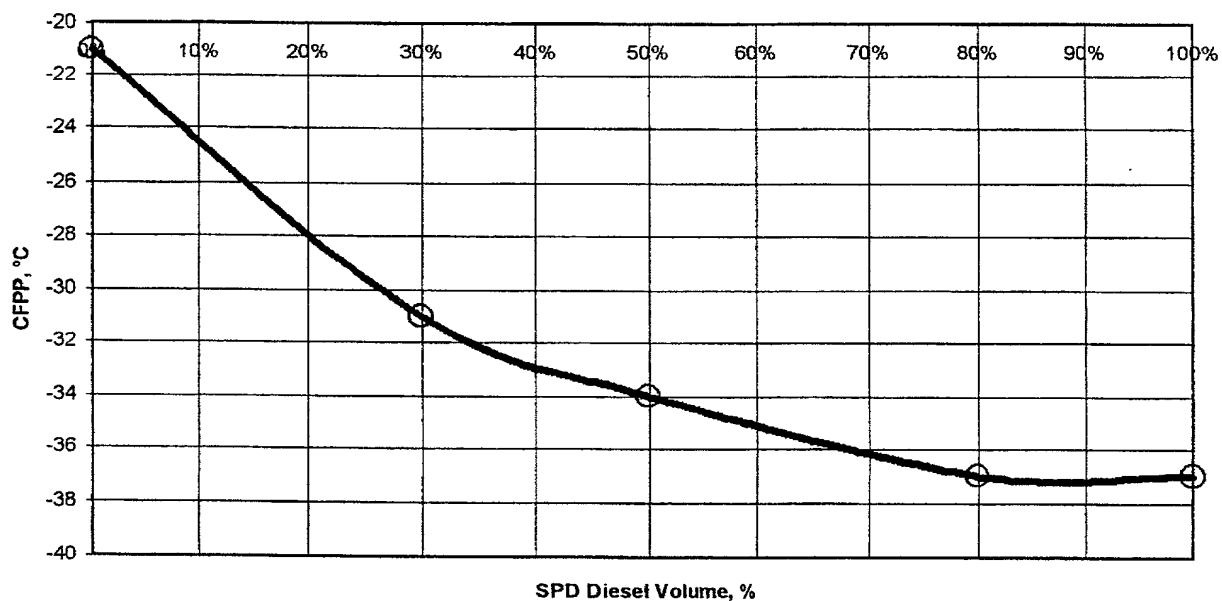
EXAMPLE 5

The diesel Blend I of Example 3 was blended with US 2-D grade diesel having desired Cetane number and CFPP properties, as shown in Table 8 and charts 1 and 2 below, were obtained.

Table: 8 Performance properties of Sasol SPD diesel, 2D diesel and blends

PROPERTY	TEST METHOD	SASOL SPD DIESEL	80:20 SPD:2D	50:50 SPD:2D	30:70 SPD:2D	US 2-D GRADE DIESEL
Cetane number	ASTM D 270	> 73.7	62.2	55.2	50.9	47 (min)
CFPP (°C)	IP 309	-37	-37	-34	-31	-21
Thermal Stability (% reflectance)	Octel F21-61 test (180 minutes, 150°C)	99.1	90	81.2	70.4	66.5
Lubricity: SL BOCLE (g) HFRR (WSD in um)	ASTM D 6078/ CEC F-06-A-96	2700 / 567	2700 / 491	3050 / 473	3650 / 491	3950 / 485

Cold flow properties of SPD diesel, 2D diesel and blends



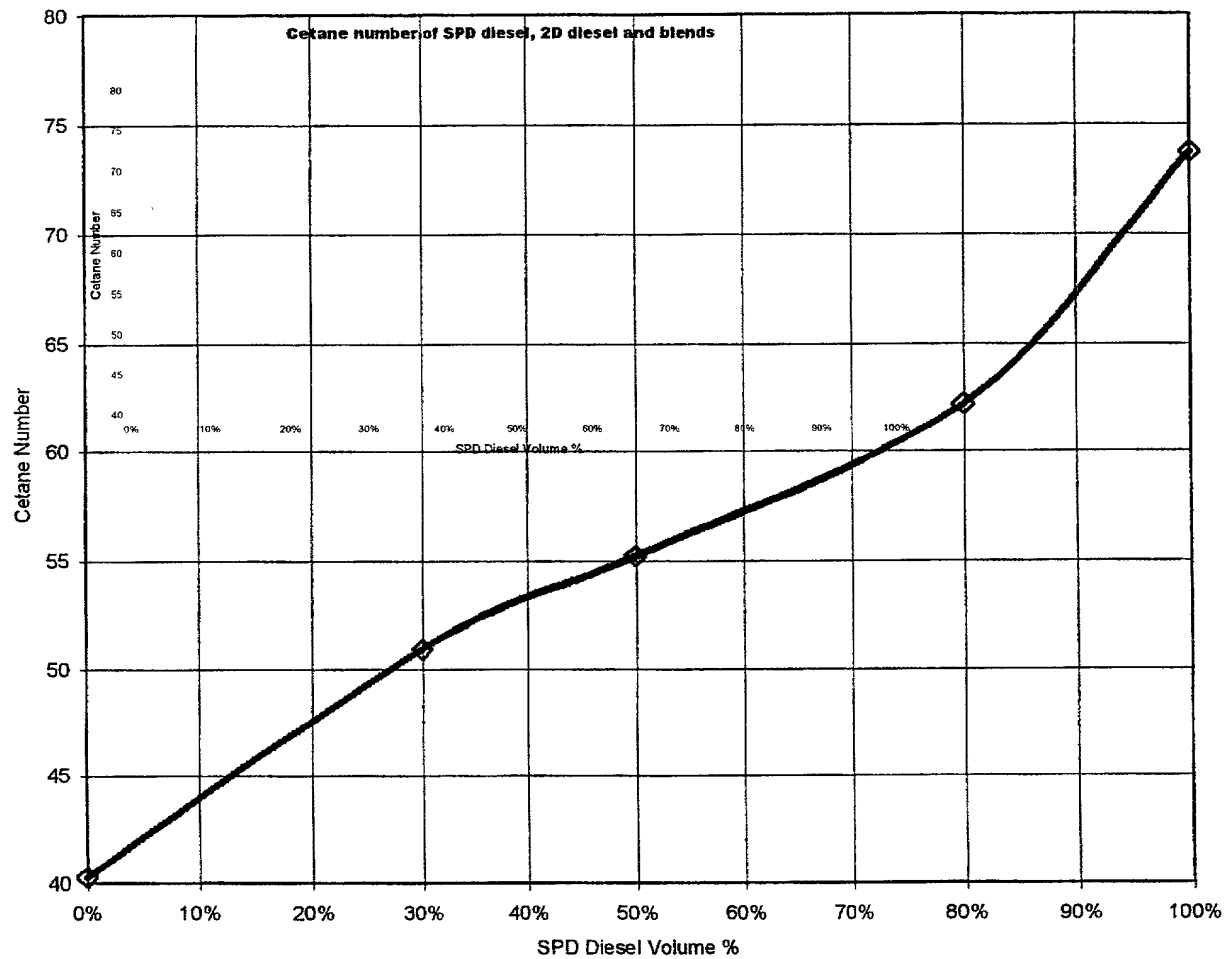
Cetane number of SPD diesel, 2D diesel and blends

Chart 2: Cetane Number of Applicants Diesel and Blends Thereof.

Claims:

1. A synthetic middle distillate cut comprising more than 50% isoparaffins, wherein the isoparaffins are predominantly methyl and/or ethyl and/or propyl branched.
- 5 2. A synthetic middle distillate cut as claimed in claim 1, wherein the gradient of an isoparaffins to n-paraffins mass ratio profile of the synthetic middle distillate cut increases from about 1:1 for C₈ to 8.54:1 for C₁₅ and decrease again to about 3:1 for C₁₈.
3. A synthetic middle distillate cut as claimed in claim 1 or claim 2, wherein a fraction of the synthetic middle distillate cut in the C₁₀ to C₁₈ carbon number range has a higher ratio of isoparaffins to n-paraffins than a C₈ to C₉ fraction of the synthetic middle distillate cut.
- 10 4. A synthetic middle distillate cut as claimed in any one of claims 2 to 3, wherein the isoparaffins to n-paraffins mass ratio of the C₁₀ to C₁₈ fraction is between 1:1 and 9:1.
5. A synthetic middle distillate cut as claimed in any one of claims 2 to 4, wherein the isoparaffins to n-paraffins mass ratio is about 8.54:1 for a C₁₅ fraction of the synthetic middle distillate cut.
- 15 6. A synthetic middle distillate cut as claimed in any one of claims 2 to 5, wherein a C₁₉ to C₂₄ fraction of the middle distillate cut has a narrow mass ratio range of isoparaffins to n-paraffins of between 3.3:1 and 5:1.
7. A synthetic middle distillate cut as claimed in any one of claims 2 to 5, wherein a C₁₉ to C₂₄ fraction of the middle distillate cut has a narrow mass ratio range of isoparaffins to n-paraffins of between 4:1 and 4.9:1.
- 20 8. A synthetic middle distillate cut as claimed in any one of the preceding claims, wherein the mass ratio of isoparaffins to n-paraffins is adjustable by controlling the blend ratio of hydrocracked to straight run components of the synthetic middle distillate cut.
- 25 9. A synthetic middle distillate cut as claimed in claim 8, wherein the isoparaffins to n-paraffins mass ratio of the C₁₀ to C₁₈ fraction having 30% straight run component is between 1:1 and 2.5:1.
10. A synthetic middle distillate cut as claimed in claim 8, wherein the isoparaffins to n-paraffins mass ratio of the C₁₀ to C₁₈ fraction having 20% straight run component is between 1.5:1 and 3.5:1.
- 30 11. A synthetic middle distillate cut as claimed in claim 8, wherein the isoparaffins to n-paraffins mass ratio of the C₁₀ to C₁₈ fraction having 10% straight run component is between 2.3:1 and 4.3:1.
12. A synthetic middle distillate cut as claimed in claim 8, wherein the isoparaffins to n-paraffins mass ratio of the C₁₀ to C₁₈ fraction having substantially only a hydrocracked component is between 4:1 and 9:1.
- 35

13. A middle distillate cut as claimed in any one of the preceding claims, wherein at least some of the isoparaffins are methyl branched.
14. A middle distillate cut as claimed in any one of the preceding claims, wherein at least some of the isoparaffins are di-methyl branched.
- 5 15. A middle distillate cut as claimed in any one of the preceding claims, wherein at least 30% (mass) of the isoparaffins are mono-methyl branched.
16. A middle distillate cut as claimed in any one of claims 1 to 15, wherein at least some of the isoparaffins are ethyl branched.
17. A middle distillate cut as claimed in any one of the preceding claims, wherein the ratio of isoparaffins to n-paraffins mass ratio is between about 1:1 to about 12:1.
- 10 18. A synthetic middle distillate cut as claimed in claim 17, wherein the isoparaffins to n-paraffins mass ratio is between about 2:1 to about 6:1.
19. A synthetic middle distillate cut as claimed in claim 18, wherein the isoparaffins to n-paraffins mass ratio is 4:1.
- 15 20. A synthetic middle distillate cut as claimed in any one of the preceding claims, having a light fraction in the boiling range 160°C to 270°C wherein the isoparaffins to n-paraffins mass ratio is between 1:2 and 4:1.
21. A synthetic middle distillate cut as claimed in claim 20, having a light fraction in the boiling range 160°C to 270°C wherein the isoparaffins to n-paraffins mass ratio is 2.2:1.
- 20 22. A synthetic middle distillate cut as claimed in any one of the preceding claims, having a heavy fraction in the boiling range 270°C to 370°C wherein the isoparaffins to n-paraffins mass ratio is between 4:1 and 14:1.
23. A synthetic middle distillate cut as claimed in claim 22, having a heavy fraction in the boiling range 270°C to 370°C wherein the isoparaffins to n-paraffins mass ratio is 21:2.
- 25 24. A synthetic middle distillate cut having a Cetane number above 70 and a CFPP, in accordance with IP 309, of below -20°C, said distillate having an isoparaffinic content substantially as claimed in any one of claims 1 to 23.
25. A synthetic middle distillate cut as claimed in any one of claims 1 to 24, wherein the synthetic distillate is derived from one or more FT primary product.
- 30 26. A diesel fuel composition including from 10% to 100% of a middle distillate cut as claimed in any one of the preceding claims.
27. A diesel fuel composition as claimed in claim 26, including from 0 to 90% of one or more other diesel fuel.
28. A diesel fuel composition as claimed in claim 26, including from 20 to 80% of one or more other diesel fuel.
- 35

29. A diesel fuel composition as claimed in any one of claims 26 to 28, including at least 20% of the middle distillate cut, the composition having a Cetane number greater than 47 and a CFPP, in accordance with IP 309, below -22°C .
30. A diesel fuel composition as claimed in claim 26, including at least 30% of the middle distillate cut, the composition having a Cetane number greater than 50 and a CFPP, in accordance with IP 309, below -22°C .
31. A diesel fuel composition as claimed in claim 26, including at least 50% of the middle distillate cut, the composition having a Cetane number greater than 52 and a CFPP, in accordance with IP 309, below -25°C .
32. A diesel fuel composition as claimed in claim 26, including at least 70% of the middle distillate cut, the composition having a Cetane number greater than 60 and a CFPP, in accordance with IP 309, below -30°C .
33. A diesel fuel composition as claimed in any one of claims 26 to claim 32, including from 0 to 10% additives.
34. A diesel fuel composition as claimed in claim 33, wherein the additives include a lubricity improver.
35. A diesel fuel composition as claimed in claim 34, wherein the lubricity improver comprises from 0 to 0.5% of the composition.
36. A diesel fuel composition as claimed in claim 35, wherein the lubricity improver comprises from 0.00001% to 0.05% of the composition.
37. A diesel fuel composition as claimed in claim 36, wherein the lubricity improver comprises from 0.008% to 0.02% of the composition.
38. A diesel fuel composition as claimed in any one of claims 28 to 37, wherein one of the other diesel fuels is US 2-D grade diesel fuel.
39. A diesel fuel composition as claimed in any one of claims 28 to 37, wherein one of the other diesel fuels is CARB grade diesel fuel.
40. A process for producing a synthetic middle distillate having a Cetane number higher than 70, the process including:
- separating the products obtained from synthesis gas via a FT synthesis reaction into one or more heavier fraction and one or more lighter fraction;
 - catalytically processing the heavier fraction under conditions which yield mainly middle distillates;
 - separating the middle distillate product of step (b) from a light product fraction and a heavier product fraction which are also produced in step (b); and
 - blending the middle distillate fraction obtained in step (c) with at least a portion of the one or more lighter fraction of step (a), or products thereof.

41. A process for producing a synthetic middle distillate as claimed in claim 40, wherein the catalytic processing of step (b) is a hydroprocessing step.
42. A process for producing a synthetic middle distillate as claimed in claim 40 or claim 41, including one or more additional step of fractionating at least some of the one or more lighter fraction of step (a), or products thereof, prior to step (d).
43. A process for producing a synthetic middle distillate as claimed in any one of claims 40 to 42, including the additional step of hydrotreating at least some of the one or more light fraction of step (a), or products thereof, prior to step (d).
44. A process for producing a synthetic middle distillate as claimed in any one of claims 30 to 43, wherein the one or more heavier fraction of step (a) boils above about 270°C.
45. A process for producing a synthetic middle distillate as claimed in 44, wherein the one or more heavier fraction of step (b) has a isoparaffins to n-paraffins mass ratio of between 4:1 and 14:1.
46. A process for producing a synthetic middle distillate as claimed in 45, wherein the one or more heavier fraction of step (b) has a isoparaffins to n-paraffins mass ratio of 21:2.
47. A process for producing a synthetic middle distillate as claimed in any one of claims 30 to 46, wherein the one or more heavier fraction of step (a) boils above about 300°C.
48. A process for producing a synthetic middle distillate as claimed in any one of claims 30 to 47, wherein the one or more lighter fraction boils in the range C₅ to the boiling point of the heavier fraction.
49. A process for producing a synthetic middle distillate as claimed in any one of claims 30 to 48, wherein the one or more lighter fraction boils in the range 160°C to 270°C.
50. A process for producing a synthetic middle distillate as claimed in any one of claims 48 or 49, wherein the one or more lighter fraction has an isoparaffins to n-paraffins mass ratio of between 1:2 and 4:1.
51. A process for producing a synthetic middle distillate as claimed in any one of claims 48 to 50, wherein the one or more lighter fraction has an isoparaffins to n-paraffins mass ratio of 2.2:1.
52. A process for producing a synthetic middle distillate as claimed in any one of claims 40 to 51, wherein the product of step (d) boils in the range 100°C to 400°C.
53. A process for producing a synthetic middle distillate as claimed in any one of claims 40 to 52, wherein the product of step (d) boils in the range 160°C to 370°C.
54. A process for producing a synthetic middle distillate as claimed in any one of claims 40 to 53, wherein the product of step (d) is a diesel fuel.
55. A process for producing a synthetic middle distillate as claimed in any one of claims 40 to 54, wherein the product of step (d) has a CFPP below -20°C.
56. A process for producing a synthetic middle distillate as claimed in claim 54, wherein the product of step (d) has a CFPP below -30°C.
57. A process for producing a synthetic middle distillate as claimed in claim 56, wherein the product of step (d) has a CFPP below -35°C.
58. A process for producing a synthetic middle distillate as claimed in any one of claims 40 to 57, wherein the product of step (d) is obtained by mixing the middle distillate fraction obtained in step (c) with at least a portion of the one or more lighter fraction of step (a), or products thereof, in a volume ratio selected to provide a diesel fuel having a required specification.

59. A process for producing a synthetic middle distillate as claimed in any one of claims 40 to 58, wherein the product of step (d) is obtained by mixing the middle distillate fraction obtained in step (c) with at least a portion of the one or more lighter fraction of step (a), or products thereof, in a volume ratio of between 1:1 and 9:1.
- 5 60. A process for producing a synthetic middle distillate as claimed in claim 59, wherein the product of step (d) is obtained by mixing the middle distillate fraction obtained in step (c) with at least a portion of the one or more lighter fraction of step (a), or products thereof, in a volume ratio of between 2:1 and 6:1.
61. A process for producing a synthetic middle distillate as claimed in any one of claims 58 to 60, wherein the product of step (d) is obtained by mixing the middle distillate fraction obtained in step (c) with at least a portion of the one or more lighter fraction of step (a), or products thereof, in a volume ratio of 84:16.
- 10
62. A synthetic middle distillate cut, substantially as herein described and illustrated.
63. A diesel fuel composition, substantially as herein described and illustrated.
64. A process for producing a synthetic middle distillate having a Cetane number higher than 70, substantially as herein described and illustrated.
- 15
65. A new synthetic middle distillate cut, a diesel fuel composition, or a new process for producing a synthetic middle distillate having a Cetane number higher than 70, substantially as herein described.

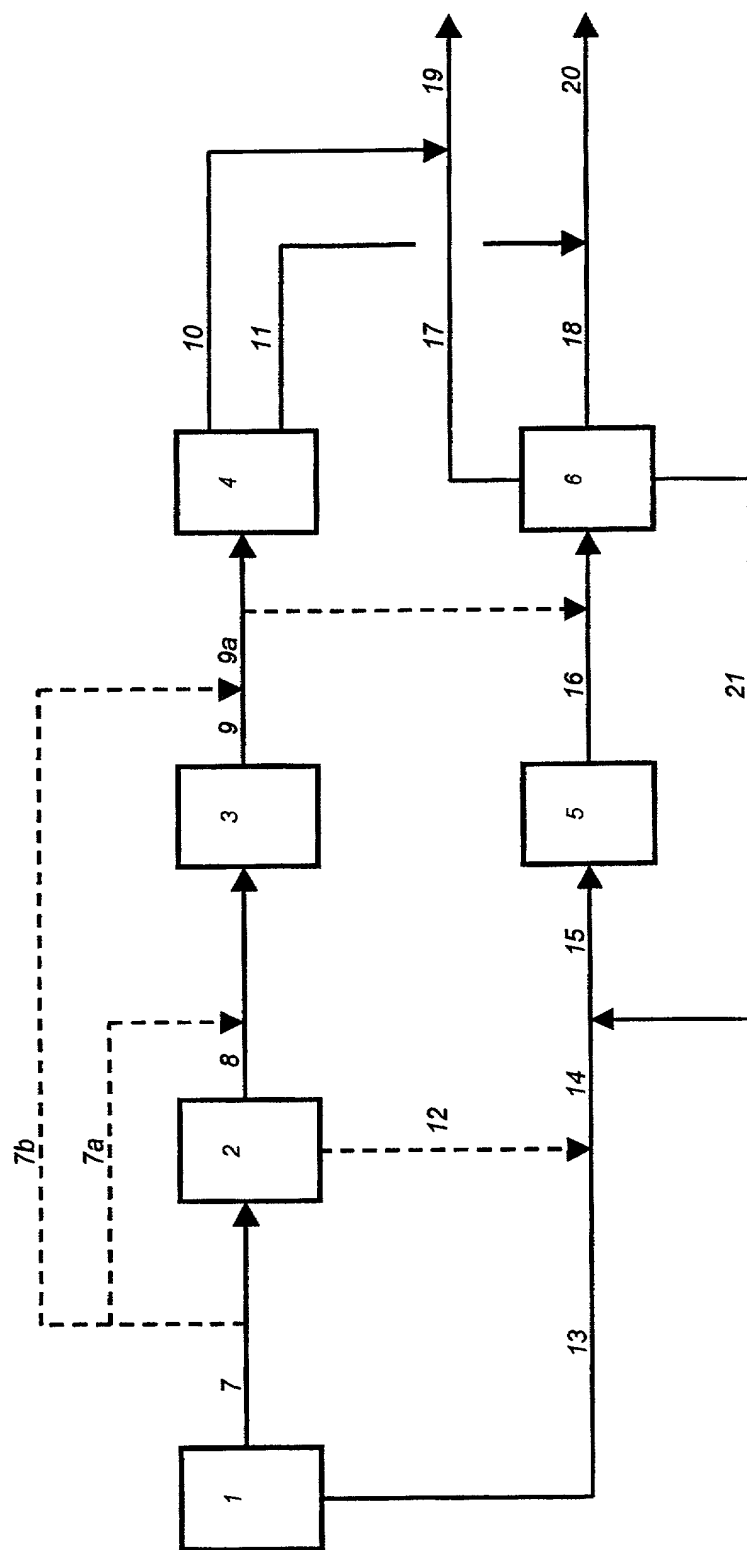


Figure 1

COMBINED DECLARATION AND POWER OF ATTORNEY FOR PATENT APPLICATION

As a below named inventor, I hereby declare that: My residence, post office address and citizenship are as stated below, next to my name. I believe I am the original, first, and sole inventor (if only one name is listed below) or an original, first, and joint inventor (if plural names are listed below) of the subject matter which is claimed and for which a patent is sought on the invention entitled "PROCESS FOR PRODUCING MIDDLE DISTILLATES AND MIDDLE DISTILLATES PRODUCED BY THAT PROCESS" the specification of which:



_____ is attached hereto.
☒ was filed on March 21, 2001
as United States Application Number 09/787,668
or PCT International Application Number _____
and was amended on _____
(if applicable)

I hereby state that I have reviewed and understand the contents of the above-identified specification, including the claim(s), as amended by any amendment referred to above. I do not know and do not believe that the claimed invention was ever known or used in the United States of America before my invention thereof, or patented or described in any printed publication in any country before my invention thereof or more than one year prior to this application, that the same was not in public use or on sale in the United States of America more than one year prior to this application, and that the invention has not been patented or made the subject of an inventor's certificate issued before the date of this application in any country foreign to the United States of America on an application filed by me or my legal representatives or assigns more than twelve months (for a utility patent application) or six months (for a design patent application) prior to this application.

I acknowledge the duty to disclose all information known to me to be material to patentability as defined in Title 37, Code of Federal Regulations, Section 1.56.

I hereby claim foreign priority benefits under Title 35, United States Code, Section 119(a)-(d), of any foreign application(s) for patent or inventor's certificate listed below and have also identified below any foreign application for patent or inventor's certificate having a filing date before that of the application on which priority is claimed:

Prior Foreign Application(s)			Priority Claimed	
<u>ZA 98/9038</u> (Number)	<u>South Africa</u> (Country)	<u>5 October 1998</u> (Day/Month/Year Filed)	<u>X</u> Yes	<u> </u> No
<u>PCT/ZA99/00096</u> (Number)	<u>PCT</u> (Country)	<u>17 September 1999</u> (Day/Month/Year Filed)	<u>X</u> Yes	<u> </u> No
<u>US 09/209,762</u> (Number)	<u>United States</u> (Country)	<u>11, December 1998</u> (Day/Month/Year Filed)	<u>X</u> Yes	<u> </u> No

I hereby claim the benefit under Title 35, United States Code, Section 119(e) of any United States provisional application(s) listed below

(Application Number)	Filing Date
_____	_____

I hereby claim the benefit under Title 35, United States Code, Section 120 of any United States application(s) listed below and, insofar as the subject matter of each of the claims of this application is not disclosed in the prior United States application in the manner provided by the first paragraph of Title 35, United States Code, Section 112, I acknowledge the duty to disclose all information known to me to be material to patentability as defined in Title 37,

Code of Federal Regulations, Section 1.56 which became available between the filing date of the prior application and the national or PCT international filing date of this application:

(Application Number)	Filing Date	(Status – patented, pending, abandoned)
(Application Number)	Filing Date	(Status – patented, pending, abandoned)
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I hereby appoint Mark R. Shanks Registration No. 33,781, Toni-Junell Herbert, Registration No. 34,348, Joseph G. Contrera, Registration No. 44,628, David W. Woodward, Registration No. 35,020, Keith D. Hutchinson, Registration No. 43,687, Shelly Guest Cermak, Registration No. 39,571, Suzannah Sundby, Registration No. 43,172, and David Steffes, Registration No. 46,042 of SHANKS & HERBERT, telephone (703) 683-3600, with a mailing address at:

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Alexandria, VA 22314

with full power of substitution and revocation, to prosecute this application and to transact all business in the Patent and Trademark Office connected herewith.

The undersigned hereby authorizes the U.S. Attorneys named herein to accept and follow instructions from undersigned's assignee, if any, and/or, if the undersigned is not a resident of the United States, the undersigned's domestic attorney, patent attorney or patent agent, as to any action to be taken in the Patent and Trademark Office regarding this application without direct communication between the U.S. attorneys and the undersigned. In the event of a change in the person(s) from whom instructions may be taken, the U.S. attorneys named herein will be so notified by the undersigned.

I hereby declare that all statements made herein of my own knowledge are true and that all statements made on information and belief are believed to be true; and further that these statements were made with the knowledge that willful false statements and the like so made are punishable by fine or imprisonment, or both, under Section 1001 of Title 18 of the United States Code and that such willful false statements may jeopardize the validity of the application of any patent issued thereon.

Full Name of Sole/First Inventor: Robert DeHaan

Inventor's Signature: _____ Date: _____

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Full Name of Second/Joint Inventor: Luis Pablo Dancuart

Inventor's Signature: _____ Date: _____

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MOP

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Inventor's Signature: MJP

Date: 23/4/2001

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Full Name of Fourth Inventor: Ewald Watermeyer DeWet

Inventor's Signature: _____

Date: _____

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Citizenship: South Africa
(Country)

Post Office Address: 24 Beethoven Street, Vanderbijlpark 1911, South Africa

TOP SECRET

MJP

COMBINED DECLARATION AND POWER OF ATTORNEY FOR PATENT APPLICATION

As a below named inventor, I hereby declare that: My residence, post office address and citizenship are as stated below, next to my name. I believe I am the original, first, and sole inventor (if only one name is listed below) or an original, first, and joint inventor (if plural names are listed below) of the subject matter which is claimed and for which a patent is sought on the invention entitled "PROCESS FOR PRODUCING MIDDLE DISTILLATES AND MIDDLE DISTILLATES PRODUCED BY THAT PROCESS" the specification of which:



is attached hereto.
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(Application Number)	Filing Date
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Full Name of Sole/First Inventor: Robert DeHaan

Inventor's Signature: Robert de Haan Date: May 9, 2001

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Post Office Address: 25 Felixstowe Street, Sasolburg 9570, South Africa

Full Name of Second/Joint Inventor: Luis Pablo Dancuart

Inventor's Signature: Luis Pablo Dancuart Date: May 9, 2001

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